- 4.16 In planning continuous casting, we use fluid flow analysis. Consider the illustrated configuration of the equipment, which includes in-line vacuum degassing.
  - a) Determine the tundish and degasser nozzle sizes which are necessary to operate the system at a rate of 6.3 kg s<sup>-1</sup> per strand. Suppose that for operational reasons it is desirable to maintain tundish and degasser bath depths of 0.76 and 1.83 m, respectively.
  - b) If only 13 mm diameter degasser nozzles are available, how would their use affect the casting operation?

Inside dimensions: tundish, 2.4 m × 2.4 m × 1.2 m; degasser, 1.2 m × 1.2 m × 2.4 m.

Liquid-steel density = 7530 kg m<sup>-3</sup>.

Discharge coefficients for tundish and vacuum degasser nozzles:  $C_D = 0.8$ . Vacuum pressure =  $10^{-3}$  atm (101 N m<sup>-2</sup>).

(a) 
$$W \coloneqq 4 \cdot 6.3 \cdot \frac{kg}{s}$$
  $h \coloneqq -0.76 \cdot m$   $\rho \coloneqq 7530 \cdot \frac{kg}{m^3}$   $Cd \coloneqq 0.8$   $P_2 \coloneqq 101 \cdot Pa$   $\beta \coloneqq 1$  
$$v_2 \coloneqq \sqrt[2]{2} \cdot Cd \cdot \left( -\frac{\left(P_2 - 1 \cdot atm\right)}{\rho} - g \cdot h \right)^{0.5} = 5.172 \frac{m}{s}$$
  $d \coloneqq \sqrt{\frac{W}{v_2 \cdot \pi \cdot \rho}} = 14.352 \text{ mm}$ 

Tundish

Vacuum

degasser

Check:

$$\frac{\langle P_2 - 1 \cdot atm \rangle}{\rho} + \frac{{v_2}^2}{2} \frac{1}{Cd^2} + g \cdot h = 0 \frac{m^2}{s^2}$$

(b) If d=13 mm Increase the head to 1.794 m to maintain the required flow rate.

$$\begin{split} W_{13} &\coloneqq W \cdot \left(\frac{13 \cdot mm}{d}\right)^2 = 20.676 \; \frac{kg}{s} \qquad v_{13} \coloneqq v_2 \cdot \left(\frac{d}{13 \cdot mm}\right)^2 = 6.303 \; \frac{m}{s} \\ f(h) &\coloneqq \frac{\left(P_2 - 1 \cdot atm\right)}{\rho} + \frac{{v_{13}}^2}{2} \; \frac{1}{Cd^2} + g \cdot h \\ h_0 &\coloneqq -1 \cdot m \qquad \qquad h_{13} \coloneqq \operatorname{root}(f(h0), h0, -0.5 \cdot m, -2 \cdot m) = -1.794 \; m \end{split}$$

Or shut down one strand and adjust head the to 0.41 m

$$\begin{split} v_3 &\coloneqq 0.75 \cdot v_{13} = 4.727 \, \frac{m}{s} & W_3 \coloneqq 0.75 \cdot W = 18.9 \, \frac{kg}{s} \\ f_3(h) &\coloneqq \frac{\left\langle P_2 - 1 \cdot atm \right\rangle}{\rho} + \frac{{v_3}^2}{2} \, \frac{1}{Cd^2} + g \cdot h & h_3 \coloneqq -0.5 \cdot m \\ h_3 &\coloneqq \operatorname{root} \left( f_3(h3), h3, -0.3 \cdot m, -2 \cdot m \right) = -0.41 \, m \end{split}$$