

SOUTH DAKOTA SCHOOL OF MINES AND TECHNOLOGY
DEPARTMENT OF MATERIALS & METALLURGICAL ENGINEERING

MET 320

Final Exam

Dec. 12, 2013

Constants:

$R = 1.987 \text{ cal/K}\cdot\text{gmole} = 8.31 \text{ J/K}\cdot\text{gmole}$

$F = 23,061 \text{ cal/volt}\cdot\text{gram equivalent} = 96,485 \text{ Joule/volt}\cdot\text{gram equivalent}$

1. Pure, liquid LiCl at 900 K is to undergo electrolysis to form Cl₂ gas at a pressure of 0.5 ATM and pure, liquid Li. What cell potential is needed? See the attached data sheets from JANAF for crystalline, liquid, and gaseous LiCl.

	<u>Melting Point, K</u>	<u>Boiling Point, K</u>
LiCl	878	1,655
Li	727	1,615

NOTE:
 (neg of Table value)
 - ΔG° form
 ↓



$\Delta G^\circ = +80,100 \frac{\text{cal}}{\text{gmole LiCl}}$
 900K

$\Delta G = \Delta G^\circ + RT \ln \frac{P_{\text{Cl}_2}^{1/2} a_{\text{Li}}}{a_{\text{LiCl}}} = (80,100 + \frac{1}{2} RT \ln \frac{1}{2})$
 ↑
 1.987 $\frac{\text{cal}}{\text{gmole K}}$

$E = \frac{\Delta G}{-nF} = \frac{\Delta G (\text{in cal})}{-(1 \text{ eq}) 23,061 \frac{\text{cal}}{\text{volt}\cdot\text{eq}}}$

$E = \frac{80,100 + \frac{1}{2} RT \ln \frac{1}{2}}{-1 * 23,061}$

$R = 1.987 \frac{\text{cal}}{\text{K}\cdot\text{gmole}}$
 $T = 900 \text{ K}$

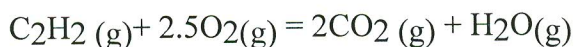
2. How many degrees of freedom are there in a system consisting of SiO_{2(s)}, CaO_(s), CaCO_{3(s)}, CO_{2(g)}, and N_{2(g)}? The silica, lime, and carbonate are all distinct phases.

$C = \begin{pmatrix} \text{SiO}_2 \\ \text{CaO} \\ \text{CaCO}_3 \\ \text{CO}_2 \\ \text{N}_2 \end{pmatrix}_5 - (\text{CaO} + \text{CO}_2 = \text{CaCO}_3)_1 - (\text{none})_0 = 4$

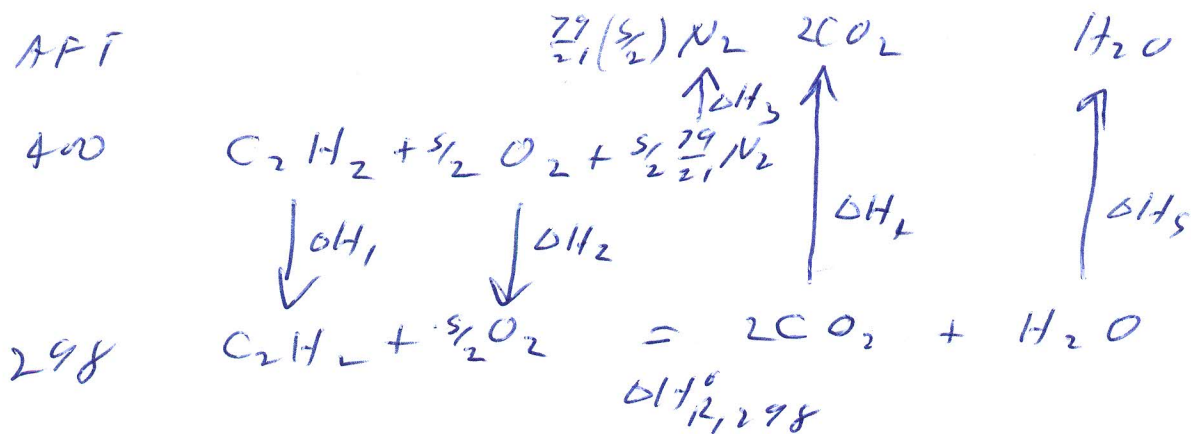
$P = \begin{pmatrix} \text{SiO}_2 \\ \text{CaO} \\ \text{CaCO}_3 \\ \text{GAS} \end{pmatrix}_4 = 4$

$F = 4 - 4 + 2 = 2$

6. Find the adiabatic flame temperature for the combustion of C_2H_2 . With air (21% O_2 and 79% N_2). The air and the C_2H_2 are initially at 400 K. Use the data provided below only.



Species	Heats of Formation (calories/g mole at 298°K)	C_p (cal/ gmole °K)
$C_2H_2(g)$	54,190	19.0
$H_2O(g)$	-57,800	10.5
$CO_2(g)$	-94,000	13.6
$O_2(g)$		8.6
$N_2(g)$		7.0



$$\sum \Delta H_s = 0$$

$$\Delta H_1 + \Delta H_2 = \int_{400K}^{298K} (C_{p,C_2H_2} + \frac{1}{2} C_{p,O_2}) dT \quad \text{see table of } C_p \text{ for values}$$

$$= (C_{p,C_2H_2} + \frac{1}{2} C_{p,O_2})(298 - 400) < 0$$

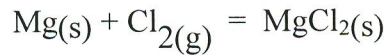
$$\Delta H_3 = \frac{79}{21} \int_{400}^{AFT} C_{p,N_2} dT = \frac{79}{21} \times \frac{1}{2} C_{p,N_2} (T_{AFT} - 400) > 0$$

$$\Delta H_{R,298}^0 = 2 \Delta H_{f,CO_2}^0 + \Delta H_{f,H_2O}^0 - \Delta H_{f,C_2H_2}^0 - \frac{1}{2} \Delta H_{f,O_2}^0 < 0$$

$$\Delta H_4 + \Delta H_5 = \int_{298}^{AFT} (2C_{p,CO_2} + C_{p,H_2O}) dT = (2C_{p,CO_2} + C_{p,H_2O}) * (T_{AFT} - 298)$$

$$\rightarrow \sum = 0 = F(T_{AFT}) \quad \text{solve } T_{AFT}$$

7. Would a gas with a partial pressure of Cl_2 of 10^{-10} atm react with solid Mg to form solid MgCl_2 at 600 K? Show your work.



see data sheet

$$\Delta G^\circ = -603,200 + 121.43 T$$

↑
600 K

$$\Delta G = \Delta G^\circ + RT \ln \frac{a_{\text{MgCl}_2}}{P_{\text{Cl}_2} a_{\text{Mg}}} = \Delta G^\circ + RT \ln 10^{-10}$$

$\frac{P_{\text{Cl}_2}}{10^{-10}}$ a_{Mg}

$$\Delta G = -603,200 + 121.43 (600) + 2.303 R T (10)$$

8.31 600
↓ ↓

appears to be < 0

∴ →

8. Show on the attached Ellingham Diagram for Ti and TiO_2 at 1000°C

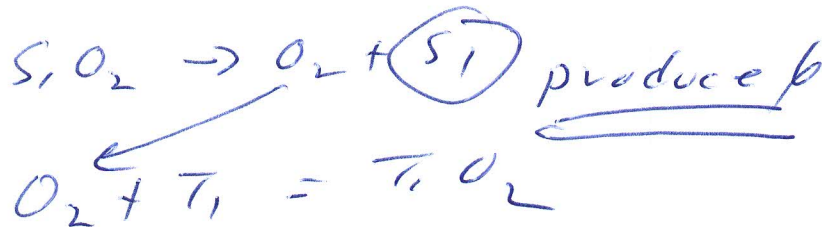
- a) the equilibrium pressure of O_2

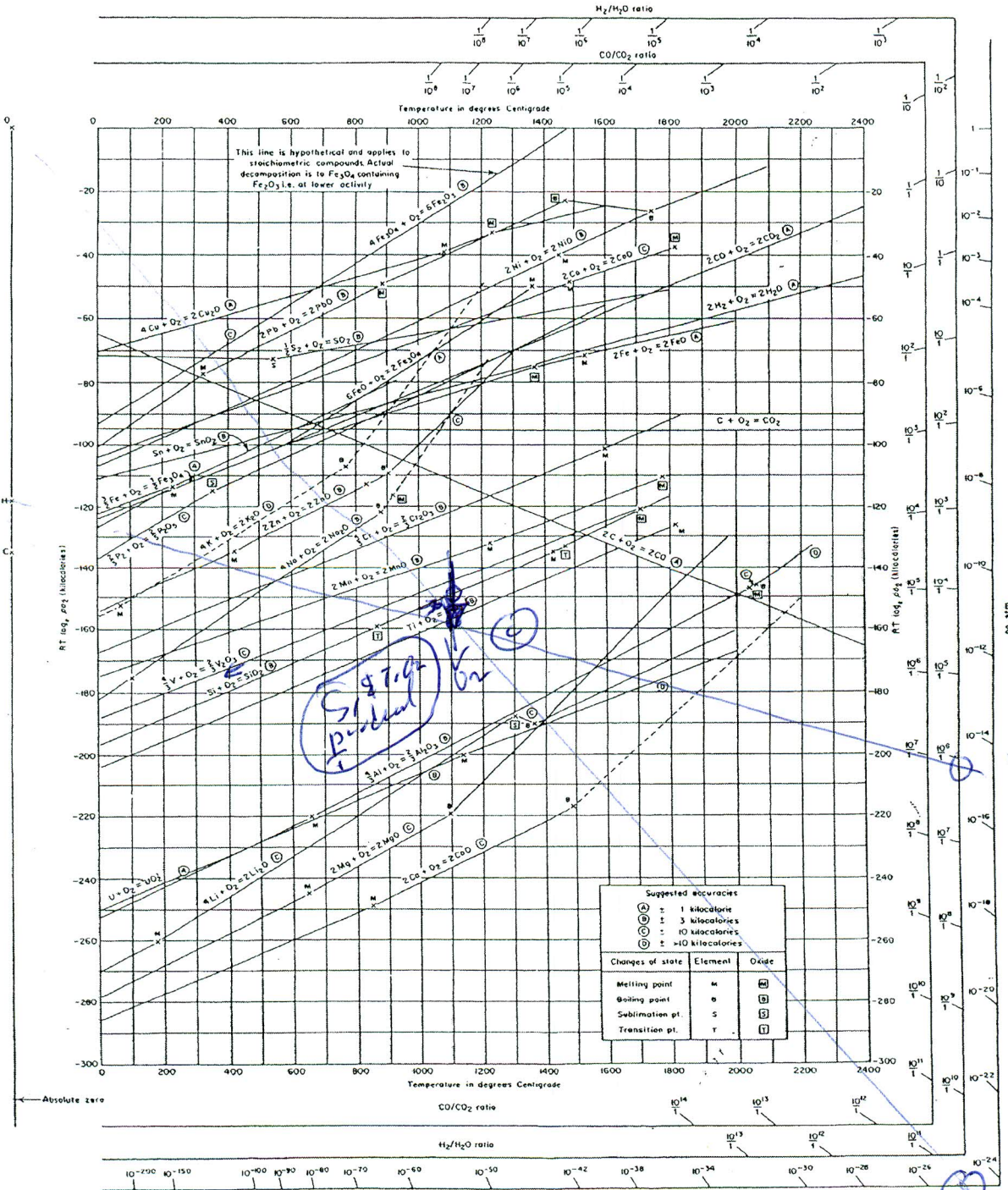
$10^{-2.5}$ atm

- b) the equilibrium $\text{H}_2/\text{H}_2\text{O}$ ratio

$10^{6.1} / 1$

- c) in the presence of Si and SiO_2 , if Ti or Si will be produced.





9.2. Based on a diagram supplied by the British Iron & Steel Research Association

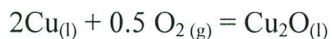
b $\frac{H_2}{H_2O} \frac{10^{-6}}{1}$

(a) 10^{-25}

9. Fill in the blank.

To obtain in a binary alloy	Given	Use Method or Equation
The Integral Molar Quantity	The Partial Molar Quantities	Tangent-Intercept method
The Partial Molar Quantity #1	The Partial Molar Quantity #2	Gibbs-Duhem eq Integration
Both Partial Molar Quantities	The Integral Molar Quantity	$\sum X_i Q_i = Q_i$

10. Show how to find the equilibrium mole fraction of Cu in a Ag-Cu alloy at 1423 K through which air is blown to form pure, liquid Cu_2O .



(See data sheet for ΔG° data.)

Activity data for liquid Ag-Cu Alloys at 1423 K

X_{Cu}	a_{Cu}
0.0	0.000
0.1	0.260
0.2	0.422
0.3	0.535
0.4	0.616
0.5	0.679
0.6	0.731
0.7	0.782
0.8	0.841
0.9	0.912
1.0	1.000

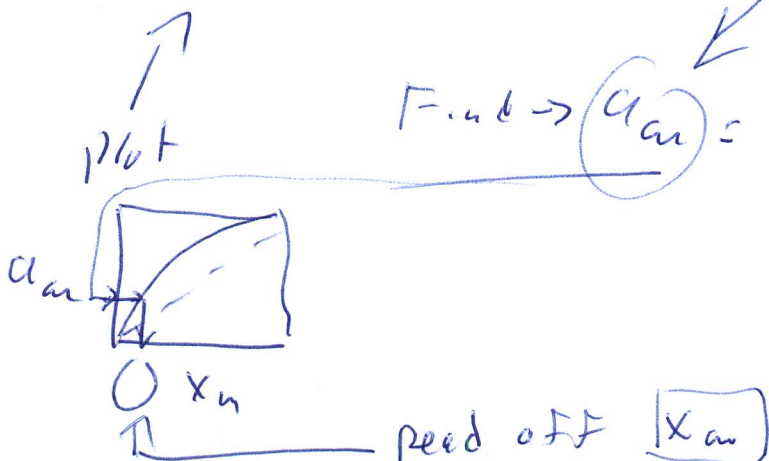
$$\Delta G^\circ = -RT \ln K_{EQ} = -1881300 + 88.98T \frac{\text{J}}{\text{mol}}$$

$\begin{matrix} 8.31 \\ \downarrow \\ 1423 \text{ K} \end{matrix}$

$$K_{EQ} = \frac{a_{\text{Cu}_2\text{O}}}{a_{\text{Cu}}^2 P_{\text{O}_2}^{1/2}}$$

$\begin{matrix} \downarrow \\ \sqrt{0.21} \end{matrix}$

Find $\rightarrow a_{\text{Cu}} = \left(\frac{1}{K_{EQ} \sqrt{0.21}} \right)^{1/2} = \gamma_{\text{Cu}} X_{\text{Cu}}$



Lithium Chloride (LiCl)

(Liquid) Mol. Wt. = 42.397

CILI

LITHIUM CHLORIDE (LiCl)

MOL. WT. = 42.397

(LIQUID)

T, °K	C _p	S° - (F° - H _{298°)/T}	H° - H _{298°}	ΔH _f	ΔF _f	Log K _f
0						
100	11.479	18.745	18.745	93.394	- 88.765	65.210
200	11.495	18.745	1.021	93.391	- 88.738	64.788
300	12.182	19.205	1.207	93.241	- 87.876	47.792
400	12.749	20.008	2.434	93.039	- 85.976	37.578
500	13.179	21.116	3.792	93.049	- 84.417	30.747
600	13.593	22.201	5.388	93.181	- 82.917	25.886
700	13.927	23.300	7.212	92.732	- 81.486	22.459
800	14.228	24.412	9.272	92.122	- 80.120	19.510
900	14.509	25.546	11.568	91.295	- 78.748	17.214
1000	14.773	26.734	14.102	91.525	- 77.471	15.391
1100	15.049	27.974	16.876	91.570	- 76.210	13.879
1200	15.324	29.274	19.898	91.425	- 74.964	12.564
1300	15.598	30.634	23.168	91.005	- 73.744	11.424
1400	15.870	32.054	26.696	90.325	- 72.552	10.457
1500	16.143	33.534	31.484	90.235	- 72.582	10.575
1600	16.414	35.074	37.532	89.987	- 71.413	9.754
1700	16.687	36.674	44.850	89.588	- 69.933	8.892
1800	16.960	38.334	53.448	89.058	- 68.107	8.017
1900	17.232	40.054	63.326	88.413	- 65.907	7.176
2000	17.505	41.834	74.484	87.563	- 63.277	6.466

ΔH_f 298.15 = -93.394 kcal. mole⁻¹
 S_{298.15} = 18.745 cal. deg.⁻¹ mole⁻¹
 ΔH_m = 4.74 ± 0.10 kcal. mole⁻¹
 T₀ (monomeric gas) = 1701°K

T_m = 883 ± 2°K
 T₀ (equilibrium mixture) = 1656°K

Heat of Formation.

Obtained from that of the crystal by adding ΔH_m and H₆₈₃-H₂₉₈(c) and subtracting H₆₈₃-H₂₉₈(l).

Heat Capacity and Entropy.

The heat capacity from the melting point to 1100°K and 1200°K has been reported by E. N. Rodigina, K. Z. Gomiński, and V. P. Luginine, Zhur. Neorg. Khim. 4, 975 (1959) and T. B. Douglas, J. L. Dever, and A. W. Haman, quoted in Natl. Bur. of Standards Report 6297. The equation given by the former authors for the enthalpy of the liquid does not agree with their measurements and has been replaced by H_m-H_{298.15} = 18.000T - 1.5 X 10⁻⁵T² - 2279 cal. mole⁻¹, which fits to ± 0.3%. The two sets of results were averaged and the equations were assumed to hold up to the normal boiling point. The entropy was calculated from that of the crystal in a manner analogous to the heat of formation.

Melting.

See table for crystal.

Boiling.

The equilibrium boiling point was taken from H. von Karmen and H. Schultz, Z. Electrochem. 27, 568 (1921) and the boiling point of the monomeric gas is defined as the temperature at which it reaches 1 atm. pressure. This was obtained from the free energy crossover between liquid and monomeric gas. The heat of vaporization to the monomeric gas was found from the tables to be 39.8 kcal. mole⁻¹.

CILI

Lithium Chloride (LiCl)

(Ideal Gas) Mol. Wt. = 42.397

T, °K.	C _p	S°	-(F°-H° ₂₉₈)/T	H°-H° ₂₉₈	ΔH°	ΔF°	Log K _p
0	0.090	0.000	INFINITE	0	0	0	INFINITE
100	9.242	42.400	8.156	46.742	46.742	46.742	1.657166
200	9.242	51.575	7.755	46.601	46.601	46.601	1.448580
298	7.946	50.864	0.000	46.778	46.778	46.778	38.081
300	7.924	50.913	0.015	46.782	46.782	46.782	37.850
400	6.332	53.235	1.700	46.008	46.008	46.008	29.312
500	5.134	55.155	1.873	46.008	46.008	46.008	24.130
600	4.677	56.705	2.434	46.291	46.291	46.291	20.623
700	4.175	58.050	3.184	46.357	46.357	46.357	18.208
800	3.687	59.252	3.922	46.379	46.379	46.379	16.268
900	3.222	60.352	4.575	46.358	46.358	46.358	14.719
1000	2.845	61.212	5.145	46.304	46.304	46.304	13.525
1100	2.541	62.067	5.736	46.248	46.248	46.248	12.583
1200	2.290	62.899	6.346	46.192	46.192	46.192	11.791
1300	2.084	63.713	6.974	46.136	46.136	46.136	11.022
1400	1.908	64.513	7.620	46.080	46.080	46.080	10.320
1500	1.757	65.295	8.284	46.024	46.024	46.024	9.686
1600	1.628	66.056	8.965	45.968	45.968	45.968	9.135
1700	1.517	66.793	9.663	45.912	45.912	45.912	8.656
1800	1.421	67.503	10.377	45.856	45.856	45.856	8.242
1900	1.337	68.183	11.106	45.800	45.800	45.800	7.892
2000	1.264	68.833	11.849	45.744	45.744	45.744	7.602
2100	1.199	69.453	12.606	45.688	45.688	45.688	7.372
2200	1.142	70.043	13.377	45.632	45.632	45.632	7.199
2300	1.092	70.603	14.162	45.576	45.576	45.576	7.072
2400	1.047	71.133	14.961	45.520	45.520	45.520	6.989
2500	1.006	71.633	15.774	45.464	45.464	45.464	6.948
2600	0.968	72.103	16.601	45.408	45.408	45.408	6.948
2700	0.933	72.543	17.442	45.352	45.352	45.352	6.972
2800	0.900	72.953	18.297	45.296	45.296	45.296	7.020
2900	0.869	73.333	19.166	45.240	45.240	45.240	7.080
3000	0.840	73.683	20.049	45.184	45.184	45.184	7.152
3100	0.812	74.003	20.946	45.128	45.128	45.128	7.236
3200	0.786	74.293	21.857	45.072	45.072	45.072	7.332
3300	0.762	74.553	22.782	45.016	45.016	45.016	7.440
3400	0.739	74.783	23.721	44.960	44.960	44.960	7.560
3500	0.717	74.983	24.674	44.904	44.904	44.904	7.692
3600	0.696	75.153	25.641	44.848	44.848	44.848	7.836
3700	0.676	75.293	26.622	44.792	44.792	44.792	7.992
3800	0.657	75.403	27.617	44.736	44.736	44.736	8.160
3900	0.639	75.483	28.626	44.680	44.680	44.680	8.340
4000	0.622	75.533	29.649	44.624	44.624	44.624	8.532
4100	0.606	75.563	30.686	44.568	44.568	44.568	8.736
4200	0.591	75.573	31.737	44.512	44.512	44.512	8.952
4300	0.577	75.563	32.802	44.456	44.456	44.456	9.180
4400	0.564	75.533	33.881	44.400	44.400	44.400	9.420
4500	0.552	75.483	34.974	44.344	44.344	44.344	9.672
4600	0.541	75.403	36.081	44.288	44.288	44.288	9.936
4700	0.531	75.293	37.202	44.232	44.232	44.232	10.212
4800	0.522	75.153	38.337	44.176	44.176	44.176	10.500
4900	0.514	74.983	39.486	44.120	44.120	44.120	10.800
5000	0.507	74.783	40.649	44.064	44.064	44.064	11.112
5100	0.501	74.553	41.826	44.008	44.008	44.008	11.436
5200	0.496	74.293	43.017	43.952	43.952	43.952	11.772
5300	0.492	74.003	44.222	43.896	43.896	43.896	12.120
5400	0.489	73.683	45.441	43.840	43.840	43.840	12.480
5500	0.487	73.333	46.674	43.784	43.784	43.784	12.848
5600	0.486	72.953	47.921	43.728	43.728	43.728	13.224
5700	0.486	72.543	49.182	43.672	43.672	43.672	13.608
5800	0.487	72.103	50.457	43.616	43.616	43.616	13.996
5900	0.489	71.633	51.745	43.560	43.560	43.560	14.388
6000	0.492	71.133	53.046	43.504	43.504	43.504	14.784
6100	0.496	70.603	54.359	43.448	43.448	43.448	15.184
6200	0.501	70.043	55.684	43.392	43.392	43.392	15.588
6300	0.507	69.453	57.021	43.336	43.336	43.336	15.996
6400	0.514	68.833	58.370	43.280	43.280	43.280	16.408
6500	0.522	68.183	59.731	43.224	43.224	43.224	16.824
6600	0.531	67.503	61.104	43.168	43.168	43.168	17.244
6700	0.541	66.793	62.489	43.112	43.112	43.112	17.668
6800	0.552	66.056	63.886	43.056	43.056	43.056	18.096
6900	0.564	65.293	65.295	42.999	42.999	42.999	18.528
7000	0.577	64.513	66.716	42.943	42.943	42.943	18.964
7100	0.591	63.713	68.149	42.887	42.887	42.887	19.404
7200	0.606	62.899	69.594	42.831	42.831	42.831	19.848
7300	0.622	62.067	71.051	42.775	42.775	42.775	20.296
7400	0.639	61.212	72.520	42.719	42.719	42.719	20.748
7500	0.657	60.352	74.001	42.663	42.663	42.663	21.204
7600	0.676	59.483	75.493	42.607	42.607	42.607	21.664
7700	0.696	58.603	77.007	42.551	42.551	42.551	22.128
7800	0.717	57.713	78.542	42.495	42.495	42.495	22.596
7900	0.739	56.813	80.099	42.439	42.439	42.439	23.068
8000	0.762	55.903	81.678	42.383	42.383	42.383	23.544
8100	0.786	55.003	83.279	42.327	42.327	42.327	24.024
8200	0.812	54.113	84.902	42.271	42.271	42.271	24.508
8300	0.839	53.233	86.547	42.215	42.215	42.215	24.996
8400	0.867	52.363	88.214	42.159	42.159	42.159	25.488
8500	0.896	51.503	89.903	42.103	42.103	42.103	25.984
8600	0.926	50.653	91.614	42.047	42.047	42.047	26.484
8700	0.957	49.813	93.347	41.991	41.991	41.991	26.988
8800	0.989	48.983	95.102	41.935	41.935	41.935	27.496
8900	1.022	48.163	96.879	41.879	41.879	41.879	28.008
9000	1.057	47.353	98.679	41.823	41.823	41.823	28.524
9100	1.092	46.553	100.502	41.767	41.767	41.767	29.044
9200	1.129	45.763	102.349	41.711	41.711	41.711	29.568
9300	1.167	44.983	104.219	41.655	41.655	41.655	30.096
9400	1.207	44.213	106.112	41.599	41.599	41.599	30.628
9500	1.249	43.453	108.028	41.543	41.543	41.543	31.164
9600	1.293	42.703	110.000	41.487	41.487	41.487	31.704
9700	1.339	41.963	112.038	41.431	41.431	41.431	32.248
9800	1.387	41.233	114.152	41.375	41.375	41.375	32.796
9900	1.437	40.513	116.343	41.319	41.319	41.319	33.348
10000	1.489	39.803	118.611	41.263	41.263	41.263	33.904

NCL. Wt. = 42.397

(IDEAL GAS)

LITHIUM CHLORIDE (LiCl)

$\Delta H_f^{298.15} = -46.742 \text{ kcal. mole}^{-1}$
 $S_{298.15}^0 = 50.864 \text{ cal. deg.}^{-1} \text{ mole}^{-1}$

$\Delta H_f^{298.15} = -46.742 \text{ kcal. mole}^{-1}$
 $S_{298.15}^0 = 50.864 \text{ cal. deg.}^{-1} \text{ mole}^{-1}$
 Ground State Configuration $1\sum$

$\omega_e = 641.1 \pm 3.0 \text{ cm.}^{-1}$
 $B_0 = 0.7053 \text{ cm.}^{-1}$
 $\omega_e x_e = 4.2 \pm 0.3 \text{ cm.}^{-1}$
 $\alpha_e = 0.0067 \text{ cm.}^{-1}$
 $\sigma = 1$
 $r_e = 2.022 \text{ \AA}$

Heat of Formation.

W. Klemperer, W. G. Morris, A. Bühler and A. G. Emslie, J. Chem. Phys. **33**, 1534 (1960) quote a private communication from W. H. Evans at the National Bureau of Standards giving $D_0 = 4.85 \text{ e.v.}$, which corresponds to $\Delta H_f^0 = -45.5 \pm 2.4 \text{ kcal. mole}^{-1}$. A third law analysis of the vapor pressure data of An. H. Nemesyany and L. A. Szalay, Zhur. Khim. **3**, 231 (1960) in conjunction with the relative concentration of monomer, dimer, and trimer at 970°K from the work of R. C. Miller and P. Kusch, J. Chem. Phys. **26**, 980 (1956) and **27**, 981 (1957) leads to a monomer heat of sublimation at 298° of 52.85 kcal. mole⁻¹, this gives $\Delta H_f^{298.15} = -45.02 \text{ kcal. mole}^{-1}$. These values lead, however, to partial vapor pressures of the monomer which are less than half of the total vapor pressure near the boiling point. From the data of Miller and Kusch *loc. cit.* it would be expected that the monomer would be the predominant species near the boiling point, a fact also substantiated by the work of C. Beaman, NBS Report OML-2323 (1957), on the average molecular weight of the vapor. Thus it was decided to change the heat of sublimation so as to give the correct normal boiling point and vapor pressures in the region 1400-1600°K and to approximate the relative concentrations of monomer, dimer, and trimer as found by Miller and Kusch at 970°K. A monomer heat of sublimation at 298° of 50.8 kcal. mole⁻¹ was chosen, which gives $\Delta H_f^{298.15} = -46.778 \text{ kcal. mole}^{-1}$. The normal boiling point was taken as 1656°K as determined by H. von Wartenburg and H. Schatz, Z. Elektrochem **27**, 568 (1921) and the boiling point of LiCl(l) was found as 1701°K from the free energy crossover between liquid and gas.

Heat Capacity and Entropy.

The spectroscopic constants were taken from Klemperer et al. *loc. cit.* The value of α_e was calculated from the value of ω_e given by the Ritz potential function and the equation given by Klemperer et al. The value of r_e was taken from the Natl. Bur. of Standards Report 6337 (1959).

Lithium Chloride (LiCl)
(Crystal) Mol. Wt. = 42.397

LITHIUM CHLORIDE (LiCl)
(CRYSTAL)

CILI

MOL. WT. = 42.397

$$\Delta H_f^{298.15} = -97.578 \pm 0.273 \text{ kcal mole}^{-1}$$

$$\Delta H_f^{298.15} = 14.173 \pm 0.015 \text{ cal deg}^{-1} \text{ mole}^{-1}$$

$$\Delta H_m = 4.74 \pm 0.10 \text{ kcal mole}^{-1}$$

$$T_m = 883 \pm 2^\circ \text{K}$$

The heat of formation was obtained as follows:

- (1) $\text{LiOH} \cdot 100\text{H}_2\text{O} + \text{HCl} \cdot 100\text{H}_2\text{O} + \text{LiCl} \cdot 20\text{H}_2\text{O}$
T. W. Richards and A. W. Rowe, *J. Am. Chem. Soc.*, **44**, 684 (1922).
- (2) $\text{Li(c)} + 100\text{H}_2\text{O(l)} + \text{LiOH} \cdot 100\text{H}_2\text{O} + 1/2 \text{H}_2(\text{g})$
S. R. Gunn and L. G. Green, *J. Am. Chem. Soc.*, **80**, 4782 (1958).
- (3) $\text{LiOH} \cdot 100\text{H}_2\text{O} + \text{LiOH} \cdot 100\text{H}_2\text{O} + 900\text{H}_2\text{O(l)}$
T. W. Richards and A. W. Rowe, *J. Am. Chem. Soc.*, **43**, 770 (1921).
- (4) $1/2 \text{H}_2(\text{g}) + 1/2 \text{Cl}_2(\text{g}) + \text{HCl}(\text{g})$
JANAF Tables.
- (5) $\text{HCl}(\text{g}) + 100\text{H}_2\text{O(l)} + \text{HCl} \cdot 100\text{H}_2\text{O}$
C. M. Slaneky, *J. Am. Chem. Soc.*, **62**, 2430 (1940), and
J. M. Sturtevant, *J. Am. Chem. Soc.*, **62**, 3265 (1940).
- (6) $\text{LiCl} \cdot 20\text{H}_2\text{O} + \text{LiCl(c)} + 20\text{H}_2\text{O(l)}$
E. Lange and F. Dürr, *Z. phys. Chem.*, **121**, 361 (1926).

$$\Delta H_{298}^{\circ} (\text{kcal mole}^{-1})$$

$$-13.704 \pm 0.014$$

$$-53.142 \pm 0.019$$

$$0.153 \pm 0.040$$

$$-21.97 \pm 0.09$$

$$-17.575 \pm 0.100$$

$$8.560 \pm 0.010$$

$$-97.578 \pm 0.273$$

A direct calorimetric determination by H. Simonsen and U. Simonsen, *Z. Electrochem.*, **55**, 643 (1952) gave -94.8 ± 0.6 kcal mole⁻¹. However, the solution route was thought to be inherently more accurate and was adopted.

Heat Capacity and Entropy

The heat capacity between 15° and 325°K has been measured by D. A. Shirley, *J. Am. Chem. Soc.*, **82**, 3841 (1960) and by F. L. Gettings, W. E. Hutton and G. C. Sinker, unpublished work, Thermal Laboratory, Dow Chemical Company. The two sets of data are in substantial agreement and were plotted together and used to evaluate the entropy at 298°. The extrapolation to 0°K was done assuming a T³ law and yielded S₁₅ = 0.019 e.u. Above 298° T. B. Douglas, J. L. Dever and A. W. Harman, quoted in Natl. Bur. Standards Report 5297, have made enthalpy measurements to 1200°K. E. M. Rodigina, K. Z. Gornalski, and V. F. Lugina, *Zhur. Neorg. Khim.*, **4**, 975 (1959) also made enthalpy determinations to 1100°K. These two sets of measurements were averaged and joined smoothly to the low temperature values.

Melting and Transition Data

The melting point has been reported as follows: 880°K., Douglas et al., loc. cit.; 883°K., Rodigina et al., loc. cit.; 883°K., H. M. Haendler, P. S. Bennett, and C. M. Wheeler, *J. Electrochem. Soc.*, **106**, 264 (1959); 879°K., H. Flood, O. Fyke and S. Urnes, *Z. Electrochem.*, **59**, 364 (1955); 879°K., H. von Martenberg and H. Schulz, *Z. Electrochem.*, **27**, 568 (1921). The highest value of 883°K. was taken as representing the most pure samples. At this temperature the enthalpy equations of Douglas et al. yield a heat of fusion of 4.718 kcal mole⁻¹, those of Rodigina et al., 4.669 kcal mole⁻¹. A. S. Dearkin and M. A. Brodigi, *J. Phys. Chem.*, **64**, 266 (1960) report a value of 4.75 ± 0.10 kcal mole⁻¹ and quote 4.83 kcal mole⁻¹ from a private communication from D. F. Smith. The average value $\Delta H_m = 4.74 \pm 0.10$ kcal mole⁻¹ was adopted.

A transition at 838°K has been reported by Kislova and Bergman, *Russ. J. Inorg. Chem.*, **5**, 1210 (1960) but is not supported by the enthalpy measurements quoted above.

T, °K.	C _p	S°	-(F°-H° ₂₉₈)/T	H°-H° ₂₉₈	ΔH _f	ΔF _f	Log K _p
0	8.679	3.207	INFINITE	2.634	97.600	97.600	INFINITE
100	10.331	9.810	15.151	1.076	97.722	93.720	102.450
298	11.479	14.173	1.000	0.000	97.578	91.786	67.278
300	11.495	14.244	0.91	0.01	97.575	91.751	66.837
400	12.182	17.652	14.633	1.267	97.523	87.671	59.079
500	12.749	20.432	15.523	2.454	96.923	87.671	50.458
600	13.267	22.894	15.584	3.756	97.868	85.857	31.272
700	13.750	25.084	16.422	5.114	97.832	83.873	26.165
800	14.325	26.749	16.822	6.514	97.858	81.662	22.379
900	14.933	28.456	17.424	7.976	97.958	81.062	19.075
1000	15.337	30.075	20.590	9.485	96.687	78.134	17.075
1100	15.819	31.560	21.821	11.043	96.265	76.299	15.158
1200	16.338	32.960	22.816	12.648	95.772	74.505	13.569
1300	16.836	34.297	23.779	14.311	95.272	72.746	12.230
1400	17.336	35.553	24.111	16.020	94.700	71.046	11.107
1500	17.831	36.766	24.914	17.778	94.076	69.372	10.107
1600	18.323	37.933	25.692	19.586	93.405	67.746	9.253
1700	18.817	39.059	26.442	21.442	92.688	66.156	8.535
1800	19.311	40.148	27.176	23.349	91.926	64.606	7.919
1900	19.805	41.205	27.887	25.305	91.123	63.100	7.416
2000	20.298	42.234	28.579	27.310	90.283	61.633	6.980